Diffusion of polystyrene in tetrahydrofuran

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The diffusion of polystyrene in tetrahydrofuran has been studied by line width measurements in a laser light scattering spectrometer. The diffusion coefficient D has been determined as a function **of** concentration c for the molecular weight range of 2.04×10^4 to 1.8×10^6 . At low concentration the relationship between D and c is linear to a very good approximation over a relatively large concentration region, as has also been found for some other systems. The molecular weight **dependence of** D, extrapolated to zero concentration, D_0 can be written as $D_0 = k_T M_W^{-b}$, where $b = 0.564$, in good agreement with thermodynamic predictions derived from intrinsic viscosity studies.

During the last few years increasing interest has arisen in the from which reliable values of the parameter k_D could be diffusional behaviour of macromolecules in solution. Experi-
mental work in particular has been highly stimulated by the region where D varies linearly with c , confirming the work mental work in particular has been highly stimulated by the region where D varies linearly with c, confirming the work development of a new measuring technique, which is also of King et al.^{1,8} and of Pusey et al.⁹ on development of a new measuring technique, which is also used here: laser light beating spectroscopy. This method, amply reviewed in the literature¹⁻³, is based on the analysis EXPERIMENTAL of the Doppler broadened spectrum of scattered light and has proven to be a very fast and reliable tool for obtaining The basic arrangement of the light beating spectrometer is accurate values for the diffusion coefficient of macro-
 $\frac{1}{3}$ accurate values for the diffusion coefficient of macro-
molecules. The same as that of some others described in literature $^{-3}$.

The free diffusion of a macromolecule in solution depends optical spectrum of scattered light by homodyning at the on both thermodynamic and hydrodynamic polymeron both thermodynamic and hydrodynamic polymer-
solvent interactions. The thermally excited concentration by measurement of its autocorrelation function. The solvent interactions. The thermally excited concentration by measurement of its autocorrelation function. The light fluctuations are the driving forces for the diffusion process, Fluctuations are the driving forces for the diffusion process, source is an ion laser (Spectra Physics, model 165) provided
which is opposed by the frictional forces exerted by the initially with a lumnter plasma tube and which is opposed by the frictional forces exerted by the initially with a krypton plasma tube and later on with an molecular surroundings. Both types of interaction depend molecular surroundings. Both types of interaction depend argon tube. Scattered light is collected with an angular
on the solute concentration c. The relationship between the concentration of 0.1^o and detected by an EMI on the solute concentration c. The relationship between the acceptance of 0.1° and detected by an EMI 9558 QB photo-
diffusion coefficient D and c is commonly written in a multiplier the The photoenreast is englised diffusion coefficient D and c is commonly written in a multiplier tube. The photocurrent is analysed by a Hewlett-
 $\frac{1}{2}$
Realized coefficient and $\frac{1}{2}$
 $\frac{2}{3}$

$$
D = D_0(1 + k_D c + \dots) \tag{1}
$$

This concentration dependence of D has been the subject function is, apart from a sharp shot noise peak at time $\tau = 0$, $\tau = 0$, $\tau = 0$, tions, but there exist striking differences between the various translational diffusion coefficient D according to: $\frac{1}{2}$ as real translational diffusion coefficient D according to: results with regard to the concentration region within which equation (1) can be approximated by the first two terms and higher terms can be neglected (linear approximation). For instance, using polarization interferometry Tsvetkov and Klenin⁴ found, in a thorough study of the diffusion of polystyrene in tetrachloromethane and butanone, a rather where λ is the wavelength in the medium and ϑ is the scatcomplicated behaviour with a concentration-independent tering angle. region at very low concentrations. Other investigators⁵⁻⁹ For all experiments the relevant part of the correlation did not observe this type of behaviour, but their measure- function was found to be given by one single exponential ments also disagree in many respects with each other. and the angular dependence of τ_c as predicted by equation Moreover, lack of sufficient accurate experimental data (2). Evidently, the translational diffusion was indeed **the** makes it difficult to verify the validity of the existing theo- only cause of the line broadening. The f'mal diffusion coef. retical expressions $\sqrt{1-x}$ for the coefficient of the linear ficient has been calculated by averaging individual values term in equation (1), k_D . **b** and the solution obtained for at least four scattering angles, usually at 20,

INTRODUCTION sion of polystyrene in the good solvent tetrahydrofuran (THF) as a function of concentration and molecular weight,

metules.
The spectrometer in essence resolves the line width of the
method is antical spectrum of estates dight by home during of the Packard correlator, model 3721 A.

In the present case the detectable part of the optical spectrum is merely determined by a symmetric, diffusional where D_0 is the diffusion coefficient at infinite dilution. broadening caused by the random motions of the scatterers, the solute macromolecules. Then the computed correlation an exponential whose characteristic time τ_c is related to the

$$
1/\tau_c = \frac{32\pi^2}{\lambda^2} \sin^2 \vartheta / 2 \times D
$$
 (2)

In this work we present experimental data of the diffu- $25, 30$ and 45° . The observed standard error of D was about

Table 1 Diffusion coefficient of a polystyrene latex (d = 109 nm) RESULTS determined at 25°C at various **wavelengths**

Wavelength, λ (nm)	Diffusion coefficient $D \times 10^8$ (cm ² /sec)			
476	4.06			
531	4.32			
568	4.31			
647	4.31			

Table 2 Temperature dependence of the diffusion coefficient of the weight $(M_w = 1.8 \times 10^6)$ this is clearer in Figure 2, where polystyrene latex (experimental and theoretical) we have replotted the data on a much larger

length range, this facility was used to test the performance macromolecules. of our equipment by measuring at four different wavelengths the diffusion of a well-defined polystyrene latex (Dow Chemical; diameter 109 nm) suspended in water. 15 The results, presented in *Table 1*, are in satisfactory agreement. The experimental diffusion coefficient compares very favourably with a value of 4.48×10^{-8} cm²/sec calculated from the Stokes-Einstein relation $(D = kT/6\pi nR)$ and even better with a reported¹³ literature value of 4.33 \times 10^{-8} cm²/sec.

For this same latex we also measured the temperature A comparison of these values with those calculated from the Stokes-Einstein relation shows that the temperature dependence of D is very well described by that relation.

For the measurements on polystyrene in THF seven samples of atactic polystyrene were used, of weight-average molecular weight M_w ranging from 2.04 \times 10⁴ to 1.8 \times 10⁶. The samples had a relatively narrow molecular weight distribution with a weight-to-number average molecular weight M_w/M_n < 1.21 according to specification. The material was supplied by Pressure Chemical Company and was used as received. Solutions were made up with distilled tetrahydrofuran containing a small amount of antioxidant, this having no effect on the measurements. The solutions were carefully filtered through $0.45 \mu m$ filters to remove disturbing dust particles. This turned out to be fully adequate: thorough examination of the shape and angular dependence of the observed correlation functions and the scattering intensity of low molecular weight samples yielded no evidence of any remaining perturbation by residual dust. Most \overline{O} 5 10 15 20 experiments were performed in the low concentration Concentration Concentration (g/l) region, i.e. up to 25 g/l for $M_w = 2.04 \times 10^4$ and up to about 10 g/1 (1%) for the highest molecular weights. For the *Figure I* Diffusion coefficient D **of polystyrene** in tetrahydrofuran to somewhat higher concentrations (4.3%) . $\qquad \qquad G, 1800000$

The experimental results for the diffusion of polystyrene in THF at low concentration are plotted in *Figure 1*. All data are obtained at λ = 647 nm at a reference temperature of 24° C. Corrections for small deviations from this average temperature during the experiments have been made according to the Stokes-Einstein relation, amounting to 2% at most.

Within the experimental error the relationship between D and c at a certain molecular weight is linear for all data shown in *Figure 1.* In the case of the highest molecular we have replotted the data on a much larger scale.

In order to obtain an indication of the range of linearity, the measurements on one sample $(M_w = 4.11 \times 10^5)$ were extended to somewhat higher concentrations (see *Figure 3*). During this experiment the krypton plasma tube of the ion laser was replaced by an argon tube and subsequently the diffusion was determined from measurements at a wavelength of 488 nm instead of 647 nm. As can be seen from *Figure 3* the two measuring series agree very well. At the highest concentrations the curve starts to deviate from a straight line; evidently the higher terms in the series expansion of equation (1) can no longer be neglected. In this region the experimental correlation function still consists of one single exponential and the angular dependence predic-1%; at low molecular weight and low concentration the ted by equation t ted by equation (2) holds very well. Thus, even with the accuracy was somewhat less. accuracy was somewhat less.
Since the krypton laser can be tuned over a wide wave-
hespadening stems from the translational diffusion of the broadening stems from the translational diffusion of the

at 24°C as a function of concentration at various molecular weights: sample of $M_w = 4.11 \times 10^5$ the experiments were extended
A, 20 400; B, 51 000; C, 97 200; D, 160 000; E, 411 000; F, 860 000;

Figure 2 Concentration dependence of the diffusion coefficient of **independent region at very low concentration⁴.**
Figure 2 Concentration dependence of the diffusion coefficient with **The relative change of the diffusi** polystyrene in tetrahydrofuran at M_W = 1.8 x 10⁶

Figure 3 Concentration dependence of the diffusion coefficient

of polystyrene in tetrahydrofuran at $M_W = 4.11 \times 10^5$: \bullet , at

488 nm, argon tube; \overline{V} ; at 647 nm, krypton tube
 \overline{V} \overline{C}

DISCUSSION
 \over **488 nm, argon tube; ▼, at 647 nm, krypton tube**

DISCUSSION ~o 2I

Extrapolated values of D at $c = 0$, D_0 , and the relative \log^4 iO \log^5 slope of the plots in *Figure 1, k_D*, have been obtained from M_w
a least-squares fit. The results are presented in *Table 3* and a least-squares fit. The results are presented in *Table 3 and Figure 4* **Diffusion coefficient of** polystyrene in tetrahydrofuran shown graphically in Figure 4. For the diffusion coefficient at infinite dilution, D_0 , and the linear coefficient of the concentra-
a double-logarithmic plot has been chosen to emphasize the tion dependence of D, k_D ,

$$
D_0 = k \, \gamma M_w^{-b} \tag{3}
$$

Values of $k_T = 3.45 \times 10^{-4}$ cm²/sec and $b = 0.564$ are 1.4 obtained with standard deviations of 0.18×10^{-4} and 0.004 respectively. The experimental values of D_0 differ from those calculated on the basis of equation (3) and the given values of k_T and b by at most 2%.

According to thermodynamic theories, the parameter b is related to the corresponding exponent a in the Mark-Houwink
relationship for the intrinsic viscosity, as relationship for the intrinsic viscosity, as

$$
b = (1 + a)/3 \tag{4}
$$

The value of $a = 0.692$ calculated from b agrees quite well \vert with the frequently cited value of 0.70 obtained by Benoit *et al.* ¹⁴ and many other reported values which, with a few exceptions, all lie in the range 0.68 to 0.70.

Concentration dependence of D

that the concentration dependence of D can be approximated by a linear relationship over a relatively large concentration range, at least up to about $c = 20$ g/l for the lower molecular weights. This result confirms the recent find ings^{$7-9$} on some comparable systems (e.g. polystyrene in O 115 115 butanone). Our data do not yield any evidence suggesting
Concentration (g/l) concentration (g/l) a more complicated behaviour with a concentrationa more complicated behaviour with a concentration-

linear coefficient of the concentration dependence of *D, k D,* **as a** function of molecular weight **for polystyrene in** tetrahydrofuran

6⊦	M_{W}	$D_0 \times 10^7$ (cm ² /sec)	k_D (I/g)	
	1 800 000	1.01	0.264	
	860000	1.59	0.136	
4⊦	411000	2.35	0.091	
	160000	3.99	0.044	
	97 200	5.43	0.028	
	51000	7.65	0.016	
2⊦	20 400	12.7	0.007	

tion dependence of *D, k _D,* as functions is of molecular weight

Table 4 Values of the second virial coefficient A₂ for polystyrene Einstein relation for diffusion, an equivalent hydrodynamic
in THF calculated using the experimental concentration dependence radius PP at infinite dil of D in the Pyun--Fixman relation (see equation 5)

inves igated. Hence it may be concluded that the increase investigated investigated. Hence it may be concluded that the increase from R_R^D , with $V_h = 4\pi/3(R_h^D)^3$. of the friction which counteracts the diffusion process is by far outweighed by the even larger increase in the thermo-
dynamic driving forces. How ver, k_D shows a remarkably hydrodynamic radii, R_h^D and R_h^n , are proportional to the dynamic driving forces. How *ver*, k_D shows a remarkably strong variation with molecular weight. At $M = 2.04 \times 10^{-4}$ radius of gyration, and their ratio is given by: 104 and a concentration of 10 g/l the relative departure of *D* from D_0 is only 7%, while at $M = 1.8 \times 10^6$ and the same concentration, the diffusion coefficient has changed by about 260% (using linear extrapolation)! Hence, especially at the higher molecular weights, great care is needed when Clearly, the assumptions of the Kirkwood-Riseman

pered by the fact that all these expressions contain the for polystyrene in THF. This may be due to excluded second virial coefficient A_2 , for which no experimental volume effects and polymer-solvent interactions, whic second virial coefficient A_2 , for which no experimental volume effects and polymer-solvent interactions, which
data are available in the present case. In the Pyun-Fixman¹¹ will lower the segment density of the coil a data are available in the present case. In the Pyun-Fixman¹¹ will lower the segment density of the coil and make it more
approximation for instance (other theories^{10,12} lead to ana-
permeable to the solvent. The effect logous relationships), the theoretical expression for k_D diffusion and viscosity. becomes:
In the literature we found some measurements on poly-

$$
k_D = 2A_2M - k_f^{\Phi} \frac{N_a V_h}{M} - v_2
$$
 (5)

(see the next section), v_2 the partial specific volume and as predicted by theory, and consequently their ratio is
N. Avogadro's number. The second term on the right. Constant. For butanone this ratio changes with mole hand side of equation (5) is an expression for the coef-
ficient of the linear term k_f in a series expansion of the value of 0.78 predicted by the Kirkwood–Riseman theory. ficient of the linear term k_f in a series expansion of the value of 0.78 predicted by the Kirkwood-Riseman theory.

The hydrodynamic radii in the very good solvent THF are
 $\frac{1}{2}$ friction coefficient. The crucial po friction coefficient. The crucial point in equation (5) is the The hydrodynamic radii in the very good solvent THF are precise value of the parameter k_f^{ϕ} , which varies from 2.23 by far the largest.

evaluated from the hydrodynamic radius for diffusion R_h^D (as discussed in the next section). Some results are given in *rable 4* for $k_f^* = 2.23$ and for the intermediate value of k_f^* = 5. Comparing these results for THF with those for another good solvent, toluene (where A_2 = 1.9 \times 10 $^{-+}$ and $\qquad\qquad$ *Table 5* \qquad The hydrodynamic radii $R_{\rm *}^D$ and $R_{\rm *}^T$ in THF and the 5.2×10^{-4} cm³ mol/g² at $M = 1.8 \times 10^{6}$ and 2.04×10^{4} unperturbed radius of gyration R^o of polystyrene respectively), we note that the calculated values of A_2 are of dependence. For determination of the best value of k_f^2 and $\frac{1}{200000}$ and $\frac{47.1}{46}$ 46 36.7 1.28 for a comparison with other theoretical expressions, experi-
 $860,000$ 29.8 30 25.4 1.18 mental data on A_2 for polystyrene in THF are required.

Hydrodynamic radius

radius R_h^D at infinite dilution can be calculated, according to:

$$
R_h^D = kT/6\pi\eta_0 D_0 \tag{6}
$$

where k is Boltzmann's constant, T the absolute temperature and η_0 the viscosity of the solvent. The results are presented in *Table 5*. In the same Table we have included 160 000 44 60 3.2 135 5.6 some other parameters: the hydrodynamic radius R_L^n derived 97 200 28 3.3 85 5.8 from viscosity measurements $(R_{\mu}^{7} = [3/n]M/10\pi N_{\mu}^{2}]^{1/3}$, 20 400 7 14 5.1 31 9.3 the intrinsic viscosity $|\eta| = 1.41 \times 10^{-2} M^{0.70}$ cm³/g) and the unperturbed radius of gyration R_g^0 obtained from light *k* D and *kf* in cm³/g; A₂ in cm³ mol/g² statted in the sected of the sectering measurements in 0-solvents, as found in ref 15. There appears to be hardly any difference between $R_{\rm h}^D$ and R_h^{η} , and their ratio is almost independent of molecular concentration, represented by the value of the parameter weight, as was already evident from the consistencies of k_D , is positive over the whole of the molecular weight range parameters a and b in the first section of t k_D , is positive over the whole of the molecular weight range parameters a and b in the first section of this Discussion.

inves igated. Hence it may be concluded that the increase The hydrodynamic volumes used in equati

$$
R_h^D/R_h^{\eta} = \frac{0.665 R_g}{0.875 R_g} = 0.76\tag{7}
$$

interpreting measurements taken at one single concentration. theory, which is based on a polymer coil with an 'ideal' seg-
A comparison of k_D with theoretical expressions is ham-
ment distribution (random flight statist ment distribution (random flight statistics), are not fulfilled permeable to the solvent. The effect may be different for

styrene in other solvents: the θ -solvent cyclohexane and the rather good solvent butanone and it is very interesting to compare the various results. This can be done from *Table 6* for the highest and lowest molecular weight of our samples. where V_h is the hydrodynamic volume per macromolecule In cyclohexane R_h^D and R_h^{η} are both proportional to $M^{\dot{1}/2}$, (see the next section), v_2 the partial specific volume and as predicted by theory, and co *N_a* Avogadro's number. The second term on the right-
hand side of equation (5) is an expression for the coef-
weight. In both cases the ratios differ considerably from the

for θ -conditions to a hard sphere value of 7.16.
We have used equation (5) to calculate A_2 inserting our radii refer to infinite dilution. At finite concentrations the We have used equation (5) to calculate A_2 , inserting our radii refer to infinite dilution. At finite concentrations the hydrodynamic volume hydrodynamic radius in a good solvent such as THF will experimental values for k_D and the hydrodynamic volume hydrodynamic radius in a good solvent such as 1 HF will
evaluated from the hydrodynamic radius for diffusion R^D decrease owing to the increase in the unfavourab

respectively), we note that the calculated values of A_2 are of the right order of magnitude and so is the molecular weight	M_{W}	R_h^D (nm)	R_B^{η} (nm)	R^0_{α} (nm)	R_B^D/R_o^0	
dependence. For determination of the best value of k_f^{Ψ} and	1800000	47.1	46	36.7	1.28	
for a comparison with other theoretical expressions, experi-	860 000	29.8	30	25.4	1.18	
mental data on A_2 for polystyrene in THF are required.	411 000	20.2	20	17.5	1.15	
	160 000	11.9	12	10.9	1.09	
	97 200	8.7	8.8	8.5	1.02	
Hydrodynamic radius	51 000	6.2	6.1	6.2	1.00	
With the experimental values of D_0 and the Stokes-	20 400	3.7	3.6	39	0.95	

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Solvent	Tetrahvdrofuran			Butanone			Cyclohexane		
D_0 (cm ² /sec) $\begin{array}{l} \n\left[\eta\right] \text{ (cm}^3/\text{g})\\ B_B^D \text{ (nm)}\n\end{array}$ R_h^{η} (nm)	$3.45 \times 10^{-4} M_W^{-0.564}$ (this work) 1.41 x 10^{-2} $M_{W}^{0.70}$ (ref 14) $1.37 \times 10^{-2} M_{W}^{0.564}$ 1.31 x 10^{-2} $M_{\rm W}^{0.567}$		$5.5 \times 10^{-4} M_W^{-0.561}$ (ref 8) 3.9×10^{-2} $M_{W}^{0.58}$ (ref 15) $0.99 \times 10^{-2} M_W^{0.561}$ 1.84×10^{-2} $M_{\rm W}^{0.523}$ Butanone			$1.3 \times 10^{-4} M_W^{-0.497}$ (ref 7) 8.4×10^{-2} $M_W^{0.50}$ (ref 15) 2.31×10^{-2} M _W ^{0.497} 2.37×10^{-2} $M_{\rm W}^{0.500}$ Cyclohexane			
	Tetrahydrofuran								
M_{W}	R_h^D	яŖ	R_h^D/R_h^{η}	R_h^D	яŖ	R_h^D/R_h^{η}	R_h^D	RЙ	R_h^D/R_h^{η}
1800000 20 400	47.1 3.7	45.8 3.6	1.03 1.03	32.0 2.6	36.1 3.4	0.89 0.76	29.7 3.2	31.8 3.38	0.93 0.94

Table 6 Comparison of hydrodynamic radii of polystyrene in various solvents

polymer interactions, the precise reduction being unknown Applications to Chemistry, Biology and Physics', Wiley, New

for this system However, by assuming the radius to remain York, 1976 for this system. However, by assuming the radius to remain $\frac{\text{York}, 1976}{\text{T}}$
constant an appropriate ortimation of the total budge of Tsyetkov, V. N. and Klenin, S. I. J. Polym. Sci. 1958, 30, 187 constant, an appropriate estimation of the total hydro- $\frac{4}{5}$ dynamic volume of the macromolecules at a given concentration can be obtained. From such an estimation it turns 6 Ford, N. C., Karasz, F. E. and Owen, J. E. M. *Discuss. Fara-*

out that. in most of our measuring series plotted in *Figure 1*. *day Soc.* 1970, 49, 228 out that, in most of our measuring series plotted in *Figure 1, day Soc.* 1970, 49, 228 there must already be a considerable overlap of the coils. Nevertheless, this has hardly any effect on the concentration 8 King, T. A., Knox, A. and Adam, J. D. G. *Polymer* 1973, 14, dependence of the diffusion coefficient, which remains 293
linear over the whole indicated region. 9 Puse

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